Example 2: Mass-Balance Only with Standard Input and a Flow Splitter and a Recycle Stream

Let's make the problem more interesting by assuming the reaction is not $100 \%$ complete, but has a fractional conversion of $80 \%$, and adding a flow splitter to recycle some of the unreacted components. The recycle stream recycles $90 \%$ of the inlet into the splitter.


Points to observe:

1. There is a tear stream created by $\mathrm{A}+$, which is RECYCLE. Notice the convergence block called \$SOLVER01.
2. The Control Panel shows iterative calculations in which the default numerical solver called Wegstein was used by A+, and the total number of iterations is 9 .
3. Can provide initial an initial guess for the tear stream (RECYCLE) by providing component flow rates ( T and P are irrelevant because we are doing mass-balance only calculations). A good initial guess can reduce the number of convergence iterations.
Try the following component flow rates ( $\mathrm{lbmol} / \mathrm{hr}$ ):
$\mathrm{CH}_{4}=90, \mathrm{O}_{2}=0, \mathrm{CO}_{2}=120, \mathrm{H}_{2} \mathrm{O}=1$, and $\mathrm{H}_{2}=80$.

We must reset the calculations, and notice that the number of iterations went from 9 to 5, thus using less computation time. Also, note how you can use Clear in the Data Browser to clear the content of the RECYCLE stream.

| Main Flowsheet $\times$ Control Panel $\times$ Results Summary - Streams (All) $\times$ SPLITTER (FSplit) $\times+$ |  |
| :---: | :---: |
| $\checkmark \square \square \mathbf{M}$ |  |
| Sequence ( | Messages |
| C萝\$OLVER01 <br> Gr REACTOR G- SEP © SPLITER | ```Flowsheet Analysis : Block $OLVER01 (Method: WEGSTEIN) has been defined to converge streams: RECYCLE \| COMPUTATION ORDER FOR THE FLOWSHEET: $Olver01 reactor sep splitter (RETURN $OLVER01) ->Calculations begin ... > Beginning Convergence Loop $OLVER01 Method: WEGSTEIN``` |


|  |  | S1 | S2 | S 3 | S 4 | S 6 | RECYCLE |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| From |  |  | REACTOR | SEP | SEP | SPLITTER | SPLITTER |
| To |  | REACTOR | SEP | SPLITTER |  |  | REACTOR |
| Stream Class |  | CONVEN | CONVEN | CONVEN | CONVEN | CONVEN | CONVEN |
| Average MW |  | 22.618092 | 23.332612 | 23.582415 | 22.171148 | 23.582415 | 23.58277 |
| Mole Flows | lbmol/hr | 100 | 385.62721 | 317.36881 | 68.258397 | 31.736881 | 285.62721 |
| CH4 | lbmol/hr | 40 | 105.26316 | 94.736842 | 10.526316 | 9.4736842 | 85.263158 |
| O 2 | lbmol/hr | 50 | 10 | 0 | 10 | 0 | 0 |
| CO 2 | libmol/hr | 0 | 137.93097 | 131.03442 | 6.8965486 | 13.103442 | 117.93097 |
| H2O | lbmol/hr | 0 | 40.733198 | 0.814664 | 39.918534 | 0.0814664 | 0.7331976 |
| H2 | lbmol/hr | 10 | 91.699882 | 90.782883 | 0.9169988 | 9.0782883 | 81.699882 |
| Mole Fractions |  |  |  |  |  |  |  |
| CH4 |  | 0.4 | 0.2729661 | 0.2985071 | 0.1542128 | 0.2985071 | 0.298512 |
| O 2 |  | 0.5 | 0.0259318 | 0 | 0.1465021 | 0 | 0 |
| CO 2 |  | 0 | 0.3576796 | 0.4128774 | 0.1010359 | 0.4128774 | 0.4128842 |
| H2O |  | 0 | 0.1056284 | 0.0025669 | 0.584815 | 0.0025669 | 0.002567 |
| H2 |  | 0.1 | 0.2377941 | 0.2860485 | 0.0134342 | 0.2860485 | 0.2860368 |
| Mass Flows | lb/hr | 2261.8092 | 8997.69 | 7484.323 | 1513.367 | 748.4323 | 6735.8808 |

