## CHE654 Design Project #1

Semester 1, 2025



#### Problem Statement

#### **Project Title**

Design, Simulation, and Economic Evaluation of Methyl Ethyl Ketone (MEK) Production from n-**Butane via n-Butene Intermediate** 

### **Background**

Methyl Ethyl Ketone (MEK) is a valuable industrial solvent used extensively in coatings, adhesives, and chemical synthesis. Its production from petrochemical feedstocks has drawn attention due to increasing demand and profitability. A viable route involves the dehydrogenation of n-butane to produce n-butene, which is subsequently partially oxidized to MEK. This pathway allows for high selectivity and integration into existing petrochemical infrastructure.

#### **Objective**

To develop and evaluate a full-scale process for MEK production from n-butane via n-butene as an intermediate using Aspen Plus for process simulation and economic analysis for feasibility assessment.

#### Scope of Work

#### 1. Process Simulation

- Develop a detailed process flow diagram (PFD) for the conversion of n-butane to MEK via n-butene.
- Simulate the process using **Aspen Plus**, including:
  - Feed preparation
  - Dehydrogenation of n-butane to n-butene
  - Oxidation of n-butene to MEK
  - Separation and purification
  - Recycle and purge systems (if applicable)
- Perform mass and energy balances.

• Conduct sensitivity analysis on temperature, pressure, and conversion rates.

#### 2. Economic Evaluation

- Estimate **capital and operating costs** using Aspen Economic Analyzer or external cost estimation tools.
- Perform financial analysis, including:
  - Net Present Value (NPV)
  - Internal Rate of Return (IRR)
  - Payback Period
  - o Cash Flow Analysis over the project lifetime (e.g., 10–20 years)
- Include assumptions on:
  - Plant capacity (e.g., tons of MEK per year)
  - Equipment cost index
  - Inflation/discount rates
  - o Raw material and utility costs
  - o Product selling price

### Process Overview and PFD

# Major Process Steps

- 1. Feed Conditioning
  - o n-Butane is compressed and preheated.
- 2. Dehydrogenation Reactor (R-101)
  - o n-Butane → n-Butene + H<sub>2</sub>
- 3. Intermediate Separation (V-101)
  - o Removal of hydrogen and light gases.
- 4. Oxidation Reactor (R-102)
  - o n-Butene +  $O_2$  → MEK + Byproducts
- 5. Cooling and Quenching
- 6. MEK Separation and Purification
  - o Distillation column(s) to recover pure MEK.

### 7. Byproduct Management and Recycle Loops

# Frocess Flow Diagram

(This can be redrawn in Aspen or a PFD editor based on units listed above.)

## **K** Aspen Plus Simulation: Required Input Data

#### 1. Components

- n-Butane (C₄H₁₀)
- n-Butene (C<sub>4</sub>H<sub>8</sub>)
- Oxygen (O<sub>2</sub>), Nitrogen (N<sub>2</sub>)
- Hydrogen (H<sub>2</sub>)
- MEK (C<sub>4</sub>H<sub>8</sub>O)
- Water (H<sub>2</sub>O), CO, CO<sub>2</sub>

#### 2. Reactions

## a. Dehydrogenation (Endothermic):

C4H10 → C4H8 + H2

- Reactor Type: RPlug
- Kinetics: Power law (literature-based) or assume conversion
- Typical Conditions: 500–600 °C, ~5–10 atm

### b. Oxidation (Exothermic):

C4H8 + 1.5O2 → C4H8O (MEK) + H2O

- Side reactions:
  - o Combustion to CO/CO<sub>2</sub>
- Reactor Type: RStoic or RPlug
- Temperature: 200–350 °C

### 3. Feed and Operating Conditions

n-Butane flow: 100–500 kmol/hr

- Air as oxidant: O<sub>2</sub>/N<sub>2</sub> (21/79 mol%)
- Heat exchangers for preheating/cooling
- Pressure: 5–20 atm (depending on stage)
- Use **Peng-Robinson EOS** or **SRK** for vapor-phase systems

## **Economic Analysis Inputs**

### **Capital Costs**

- Equipment sizing and costing using Aspen Plus or external references
- Installation factors
- Contingency and indirect costs

## **Operating Costs**

- Raw materials: n-Butane, air, water
- Utilities: Steam, cooling water, electricity
- Labor, maintenance, overhead

## **Revenue Assumptions**

- Market price of MEK (e.g., \$1.5–\$2.0/kg)
- Byproduct credit (e.g., hydrogen)

#### **Financial Parameters**

• Project life: 10-20 years

• Discount rate: 8-12%

• Tax rate: 25–30%

• Depreciation: Straight-line or MACRS

## **ii** Expected Deliverables

- 1. Aspen Plus flowsheet with convergence
- 2. Stream and utility tables
- 3. Equipment sizing report
- 4. Economic indicators:
  - Capital investment summary

- o Operating cost breakdown
- o NPV, IRR, Payback Period
- o Annual cash flow chart
- 5. Optimization results (if applicable)
- 6. Sustainability or environmental assessment (optional)

Would you like help building a **starter Aspen Plus file**, **sample cash flow sheet in Excel**, or assistance with **reaction kinetics estimation** from literature?