CHE654 Design Project #4

Semester 1, 2025



Problem Statement

Project Title

Simulation and Economic Evaluation of Phenol Production from Benzene and Propylene via the Cumene Process Using Aspen Plus

Background

Phenol (C₆H₅OH) is an essential industrial chemical used in the production of bisphenol A, caprolactam, phenolic resins, and other derivatives. The dominant industrial method for phenol production is the Hock process, where benzene and propylene react to form cumene, which is then oxidized to cumene hydroperoxide and subsequently cleaved to produce phenol and acetone.

This project aims to simulate the phenol production process in Aspen Plus, analyze its technical feasibility via mass and energy balances, and assess the economic viability through financial indicators such as IRR, NPV, and payback period.

Objectives

- 1. Simulate the production of phenol from benzene and propylene through the cumene (Hock) process using Aspen Plus.
- 2. Develop a **detailed process flow diagram (PFD)** including all major unit operations.
- 3. Perform **material and energy balances** to determine process efficiency.
- 4. Generate stream tables and key operating parameters for simulation units.
- 5. Conduct an **economic evaluation** using:
 - Internal Rate of Return (IRR)
 - Net Present Value (NPV)
 - Payback Period
 - **Cash Flow Analysis**
- 6. Evaluate the **financial viability** of the process and provide recommendations for scale-up or optimization.

Process Description

Main Reaction Steps:

1. Alkylation:

 C_6H_6 (benzene) + C_3H_6 (propylene) \rightarrow $C_6H_5CH(CH_3)_2$ (cumene)

2. Oxidation:

 $C_6H_5CH(CH_3)_2 + O_2 \rightarrow C_6H_5C(CH_3)_2OOH$ (cumene hydroperoxide)

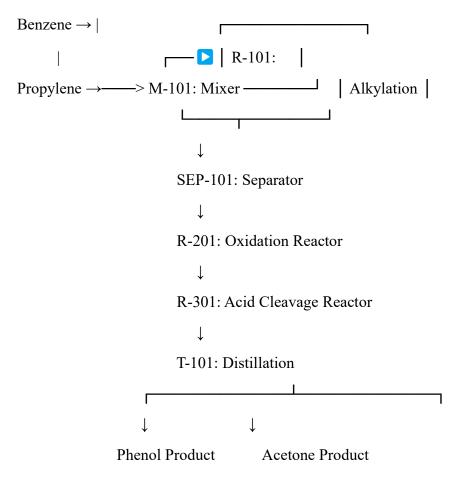
3. Cleavage (Acid-Catalyzed):

 $C_6H_5C(CH_3)_2OOH \rightarrow C_6H_5OH \text{ (phenol)} + CH_3COCH_3 \text{ (acetone)}$

• **Byproducts**: α-methylstyrene, acetophenone, and tars (in small amounts)

E Conceptual Process Flow Diagram (PFD)

FEEDS:



Aspen Plus Simulation Setup

1. Thermodynamic Model

- Use Peng-Robinson (PR) or NRTL for handling non-ideal liquid/vapor behavior.
- Use **RK-Aspen** or **SRK** for initial approximations in hydrocarbon systems.

2. Components

Component	Formula	Role
Benzene	C ₆ H ₆	Feed
Propylene	C ₃ H ₆	Feed
Cumene	C9H12	Intermediate
Cumene Hydroperoxide	C ₉ H ₁₂ O ₂	Intermediate (in Aspen: may require hypothetical compound)
Phenol	C ₆ H ₅ OH	Product
Acetone	CH ₃ COCH ₃	Co-product
Oxygen	O_2	Oxidant
Water, N ₂	Miscellaneous Side products / purge gases	

3. Typical Operating Conditions

Unit Temperature (°C) Pressure (bar) Description

Alkylation 200-250	20–30	Acid catalyst (e.g., zeolite or phosphoric acid)
Oxidation 100-140	3–6	Air/O ₂ bubbled through cumene
Cleavage 50–80	~1–2	H ₂ SO ₄ catalyst used
Distillation 80–200	~1	Separation of phenol, acetone

📊 Input Data for Aspen Simulation

A. Feed Data (Example Basis)

Component Flowrate (kmol/h) Purity (%) Source

Benzene	100	99.9	Purchased
Propylene	100	99.5	Purchased
Air/O ₂	150	21% O ₂	Utility
Catalyst	_	Fixed bed	Reactor input only

These values can be scaled depending on target phenol production (e.g., 10,000–50,000 TPA).

6 Economic Evaluation Framework

A. Capital Expenditure (CapEx)

- Reactor vessels (alkylation, oxidation, cleavage)
- Separators and distillation columns
- Heat exchangers, pumps, and utilities
- Catalyst loading and infrastructure
- Contingency and installation

B. Operating Expenditure (OpEx)

- Raw materials (benzene, propylene, air)
- Catalyst replacement
- Utilities: steam, cooling water, electricity
- Labor, maintenance, and waste handling

C. Financial Indicators

Metric	Purpose	
IRR	Return rate based on project cash flows	
NPV	Net present value over project life	
Payback Period Time to recover initial investment		
Cash Flow	Annual revenue minus expenses over time	

D. Economic Assumptions (Example)

Parameter Value

Project Life 15–20 years

Discount Rate 10%

Construction Time 2 years

Operating Days/year 330

Plant Capacity 20,000–50,000 TPA

Depreciation Straight-line (10 yrs)

Deliverables

- 1. Aspen Plus Simulation File (.bkp)
 - o Material & energy balance, flowsheets
- 2. Process Flow Diagram (PFD)
- 3. Stream Tables & Equipment List
- 4. Utility & Catalyst Consumption Estimates
- 5. Economic Model (Excel/Spreadsheet):
 - o IRR, NPV, Payback, Cash Flows
- 6. Report Summary:
 - Technical description
 - o Economic conclusions
 - o Sensitivity analysis (raw material price, scale, utility cost)